

Effect of Chemical Reaction on Mass Distribution of a Binary Fluid Mixture in Unsteady MHD Couette Flow

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ABSTRACT: The problem of mass distribution in an unsteady two dimensional flow of a viscous, incompressible, thermally and electrically conducting binary fluid mixture between two infinite vertical parallel plates under the influence of chemical reaction, uniform magnetic field and temperature gradient is studied. The magnetic field lines are assumed to be fixed relative to the moving plates. The governing partial differential equations are first transformed into ODEs by the method of separation of variables and then solved numerically by using MATLAB's built in solver bvp4c. The solution for the concentration of the rarer and lighter component of the binary fluid mixture for different values of Reynolds number, chemical reaction parameter, Schmidt number, thermal diffusion number and Peclet number are presented graphically to analyse their effects on mass distribution of the components of the binary fluid mixture.

KEYWORDS: Binary fluid mixture, unsteady, MHD Couette flow, magnetic field, chemical reaction, mass distribution

I. INTRODUCTION

MHD Couette flow between two parallel plates is a classical problem that has important applications in various industrial processing such as power generators and MHD pumps used in chemical energy technology, accelerators, aerodynamics heating, polymer technology, petroleum technology and also in many material processing applications. Heat and mass transfer problems with chemical reaction are of great importance in several processes. The effect of chemical reaction depends upon whether the reaction is homogeneous or heterogeneous. In well-mixed systems, the reaction is heterogeneous if it takes place in the interface and homogeneous if it takes place in solution. In most cases the reaction rates depends upon the concentration of species. A reaction is said to be of first order if the rate of reaction is directly proportional to the species concentration. When fluid moves through a magnetic field then an electric current may be induced and in turn current interacts with the magnetic field to produce a body force on fluid. The influence of a magnetic field in viscous incompressible flow of electrically conducting fluid is used in plastic technology to manufacturing of rayon, nylon etc.

In a binary fluid mixture the diffusion of individual species takes place by three mechanisms namely ordinary diffusion, baro-diffusion and thermo-diffusion. The diffusion flux \mathbf{i} of rarer and lighter components is given by Landau and Lifshitz [1] as

$$\mathbf{i} = -\rho D[\nabla c + k_p \nabla p + k_T \nabla T] \quad (1)$$

where ρ is the density of the binary fluid mixture, $k_p D$ is the baro-diffusion coefficient, $k_T D$ is the thermo-diffusion coefficient and c is the concentration of rarer and lighter components of the binary fluid mixture. The ordinary diffusion to the mass flux is seen to depend in a complicated way on the concentration gradients of the components present in the mixture. If there is a pressure gradient imposed on the system then baro-diffusion shows that there may be a net movement of the components in the mixture. Thermal diffusion indicates the tendency for species to diffuse under the influence of a temperature gradient. It was shown by Groot and Mazur [2] that if separation due to thermal

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diffusion occurs then it might even render an unstable system to stable one. This effect is quite small, but devices can be arranged to produce very steep temperature gradients so that separation of mixtures are affected. Bodosa et al. [3] analysed the heat transfer between two horizontal plates in presence of a uniform magnetic field. Sharma and Singh [4, 5] studied analytically the Soret effect on de-mixing of species in hydro-magnetic flow of a binary mixture of incompressible viscous fluid between two parallel plates, first taking the plates horizontal and second by taking the plates vertical. Attia, H. A. [6] studied the effect of variable properties on the unsteady Couette flow with heat transfer considering the Hall Effect. Sharma et al. [7, 8, 9] investigated analytically the effect of magnetic field on separation of binary fluid mixture for different geometries. Das and Jana [10] investigated heat and mass transfer effects on unsteady MHD free convective flow near a moving vertical plate in porous medium. Sharma et al. [11, 12, 13] studied the effects of axial and radial magnetic field on de-mixing of a binary fluid mixture. Sharma, Singh and Gogoi [14] discussed the effects of magnetic field and temperature gradient on separation of a binary fluid mixture in unsteady Couette flow analytically. They did not consider the effect of chemical reaction in their investigations.

The aim of this research paper is to investigate numerically the effect of chemical reaction on mass distribution in unsteady, incompressible, viscous, electrically conducting binary fluid mixture between two infinite vertical parallel plates both of which are moving with equal velocities in opposite directions.

II. MATHEMATICAL MODELLING

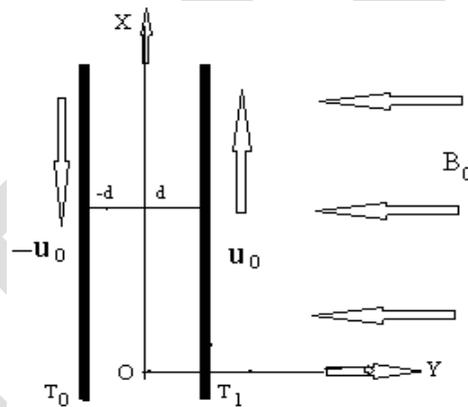


Figure 1: Schematic representation and coordinate system of the problem

The unsteady MHD flow of an incompressible viscous electrically conducting fluid between two infinite vertical parallel plates at a distance $2d$ apart is considered under the influence of a uniform transverse magnetic field. The flow is assumed to be along the X-direction, which is in the vertical direction through the central line of the channel and Y-axis is along the horizontal direction [see Fig 1]. The plates of the channel are at $y = \pm d$ and that the relative velocity between the two plates is $2u_0$. A uniform magnetic field of strength B_0 is applied perpendicular to the plates. The plate $y = -d$ is maintained at temperature T_0 , while the temperature of the plate at $y = d$ varies exponentially with time having initial temperature T_1 ($T_1 > T_0$). Since the plates are considered infinite in X- direction, hence all the physical quantities will be independent of x . Therefore all the physical variables become functions of y and t only.

We make the following assumptions:

- The magnetic field is weak. The magnetic field lines are assumed to be fixed relative to the moving plates.
- Boussinesq approximation is applied.
- Plates are non-conducting.
- No pressure gradient in the flow field.

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- No applied voltage and hence electric field is absent.

Under the above assumptions the governing equations are

$$\frac{\partial u}{\partial t} = \nu \frac{\partial^2 u}{\partial y^2} - \frac{\sigma B_0^2}{\rho} u + \bar{g} \beta_T (T - T_0) + \bar{g} \beta_c (c - c_{w1}), \quad (2)$$

$$\frac{\partial T}{\partial t} = \frac{k}{\rho c_p} \frac{\partial^2 T}{\partial y^2} \quad (3)$$

$$\text{and } \frac{\partial c}{\partial t} = D \left[\frac{\partial^2 c}{\partial y^2} + S_T \frac{\partial}{\partial y} \left\{ (c - c_{w1}) \frac{\partial T}{\partial y} \right\} \right] - k_1 (c - c_{w1}) \quad (4)$$

where u is the velocity in x - direction, ν is the kinematic viscosity, \bar{g} is the acceleration due to gravity, ρ is the density of the binary fluid mixture, β_T is the volumetric coefficients of thermal expansion, β_c is the volumetric mass expansion coefficient, σ is the electric conductivity, T is the temperature of the binary fluid mixture inside the thermal boundary layer, k is the thermal conductivity, c_p is the specific heat at constant pressure, c is the concentration of rarer and lighter components of the binary fluid mixture, D is the mass diffusion coefficient, S_T is the Soret coefficient and k_1 is the chemical reaction rate constant.

The boundary conditions of the problem are

$$u = -u_0, T = T_0, c = c_{w1} \quad \text{at } y = -d \quad (5)$$

$$\text{and } u = u_0, T = T_1 + (T_1 - T_0)\epsilon e^{-nt}, c = c_{w2} \quad \text{at } y = d \quad (6)$$

where $u_0, T_0, T_1, c_{w1}, c_{w2}$ and n are constants.

On introducing the non-dimensional quantities

$$u^* = \frac{u}{u_0}, y^* = \frac{y}{d}, t^* = \frac{tu_0}{d}, T^* = \frac{T - T_0}{T_1 - T_0}, c^* = \frac{c - c_{w1}}{c_{w2} - c_{w1}} \quad (7)$$

into equations (2) to (6) we get the following non-dimensional equations

$$\frac{\partial u^*}{\partial t^*} = \frac{1}{Re} \frac{\partial^2 u^*}{\partial y^{*2}} - Re M^2 u^* + \frac{Gr}{Re^2} T^* + Re G_c c^*, \quad (8)$$

$$\frac{\partial T^*}{\partial t^*} = \frac{1}{Pe} \frac{\partial^2 T^*}{\partial y^{*2}} \quad (9)$$

and

$$Re Sc \frac{\partial c^*}{\partial t^*} = \left[\frac{\partial^2 c^*}{\partial y^{*2}} + t \frac{\partial}{\partial y^*} \left(c^* \frac{\partial T^*}{\partial y^*} \right) \right] - \gamma c^* \quad (10)$$

together with the boundary conditions:

$$u^* = -1, T^* = 0, c^* = 0 \quad \text{at } y^* = -1 \quad (11)$$

and

$$u^* = 1, T^* = 1 + \epsilon e^{-nt}, c^* = 1 \quad \text{at } y^* = 1 \quad (12)$$

where

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$$\text{Re} = \frac{du_0}{\nu}, M^2 = \frac{\sigma B_0^2 \nu}{\rho u_0^2}, \text{Gr} = \frac{d^3 \bar{g} \beta_T (T_1 - T_0)}{\nu^2}, \gamma = \frac{k_1 d^2}{D}, \text{Sc} = \frac{\nu}{D}, \text{Gr}_c = \frac{\bar{g} \nu \beta_c (c_{w2} - c_{w1})}{u_0^3},$$

$$\text{Pr} = \frac{\nu \rho c_p}{k}, \text{Pe} = \text{Pr} \cdot \text{Re}, t_d = S_T (T_1 - T_0) \tag{13}$$

are Reynolds number, Hartmann number, Grashof number, Chemical reaction parameter, Schmidt number, Mass Grashof number, Prandtl number, Peclet number and thermal diffusion number respectively.

III. SOLUTION OF THE PROBLEM

Equations (8)-(10) represent a set of partial differential equations and cannot be solved in closed form. However, it can be reduced to a set of coupled non-linear ordinary differential equations in dimensionless form by using the following transformations:

$$u^* = f_0 + \epsilon f_1 (y^*) e^{-nt}, \tag{14}$$

$$T^* = g_0 + \epsilon g_1 (y^*) e^{-nt} \tag{15}$$

$$\text{and } c^* = h_0 + \epsilon h_1 (y^*) e^{-nt} \tag{16}$$

With the help of these transformations equations (8) to (10) with the boundary conditions (11) and (12) become

$$f_0'' - \text{Re}^2 M^2 f_0 = -\frac{\text{Gr}}{\text{Re}} g_0 - \text{Re}^2 \text{Gr}_c h_0, \tag{17}$$

$$f_1'' + \text{Re} \{n - \text{Re} M^2\} f_1 = -\frac{\text{Gr}}{\text{Re}} g_1 - \text{Re}^2 \text{Gr}_c h_1, \tag{18}$$

$$g_0'' = 0, \tag{19}$$

$$g_1'' + n \text{Pe} g_1 = 0, \tag{20}$$

$$h_0'' + t_d (h_0' g_0' + h_0 g_0'') - \gamma h_0 = 0 \tag{21}$$

$$\text{and } h_1'' + t_d h_1' g_0' + (t_d g_0'' + n \text{Re} \text{Sc}) h_1 + t_d (h_0' g_1' + h_0 g_1'') - \gamma h_1 = 0 \tag{22}$$

with the boundary conditions

$$f_0 = -1, f_1 = 0, g_0 = 0, g_1 = 0, h_0 = 0, h_1 = 0 \quad \text{at } y^* = -1 \tag{23}$$

$$\text{and } f_0 = 1, f_1 = 0, g_0 = 1, g_1 = 1, h_0 = 1, h_1 = 0 \quad \text{at } y^* = 1 \tag{24}$$

Here primes represent ordinary differentiation with respect to y^* .

Equations (14) to (19) are highly coupled and nonlinear ODE^s. So their solution in closed form is not possible. Hence we solved the equations numerically by using MATLAB's built in solver bvp4c.

IV. RESULTS AND DISCUSSIONS

Numerical calculations have been carried out for concentration of the rarer and lighter component of the binary fluid mixture for various values of the parameters Re, Pe, Sc, γ and t_d .

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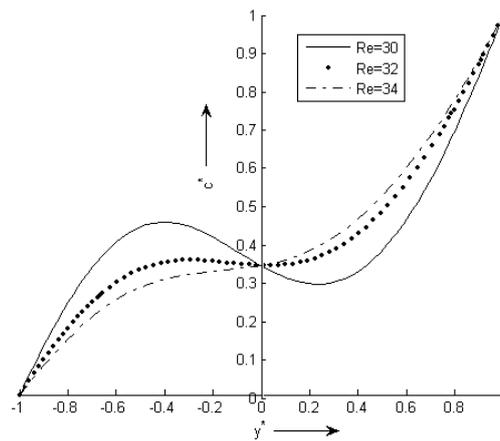


Figure 2: Concentration profile c^* against the width of the channel y^* for different values of Re and $Pe=6$; $Sc=0.2$; $t_d=0.5$; $n=2$; $\epsilon=0.2$; $Gr_c=2$; $Gr=2$; $M=1$; $t=0.5$; $\gamma=1$

Figure 2 reveals that increase in the value of Reynolds number (Re) decreases the concentration of the rarer and lighter component of the binary fluid mixture at any point in the region $[-1, 0]$ and increases the concentration of the rarer and lighter component of the binary fluid mixture at any point in the region $[0, 1]$. Thus the concentration of the rarer and lighter component of the binary fluid mixture can be increased by increasing the value of the Reynolds number (Re) i.e. with the increase in the value of density of the mixture, with the increase in the values of the magnitude of velocity of the plates, with the increase in the values of the distances between the plates, and with the decrease in the viscosity of the fluid mixture.

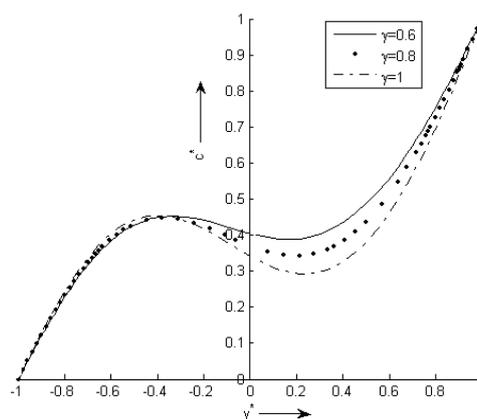


Figure 3: Concentration profile c^* against the width of the channel y^* for different values of chemical reaction parameter γ and $Re=30$; $Pe=6$; $t_d=0.5$; $Sc=0.2$; $n=2$; $\epsilon=0.2$; $Gr_c=2$; $Gr=2$; $M=1$; $t=0.5$

Figure 3 signifies that if the value of the chemical reaction parameter γ increases then there is a little increase in the concentration of the rarer and lighter component of the binary fluid mixture in the region $-1 \leq y^* \leq -0.344$ and then decreases in the region $-0.344 \leq y^* \leq 1$. Thus by decreasing the value of chemical reaction parameter γ the concentration of the rarer and lighter component in the binary fluid mixture can be increased.

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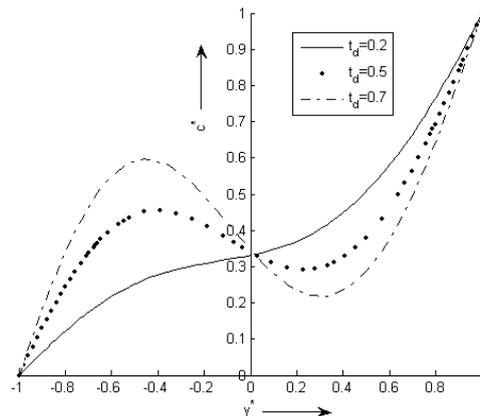


Figure 4: Concentration profile c^* against the width of the channel y^* for different values of t_d and $Re=30$; $Pe=6$; $Sc=0.2$; $n=2$; $\epsilon=0.2$; $Gr_c=2$; $Gr=2$; $M=1$; $t=0.5$; $\gamma=1$

Figure 4 depicts that as the value of the thermal diffusion parameter t_d increases the concentration of the rarer and lighter component of the binary fluid mixture increases sharply at any point in the region $y^* \leq 0$ and there is a sharp decrease in the concentration of the rarer and lighter component of the binary fluid mixture at any point in the other half of the channel. Thus by increasing in the value of thermal diffusion parameter t_d which depends on Soret number and temperature gradient between the two plates can increase the concentration of the rarer and lighter component of the binary fluid mixture at any point in the region $[-1, 0]$ and can decrease the concentration of the rarer and lighter component of the binary fluid mixture in the region $[0, 1]$.

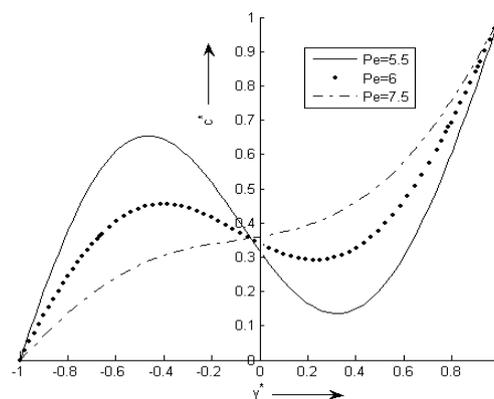


Figure 5: Concentration profile c^* against the width of the channel y^* for different values of Pe and $Sc=0.2$; $Re=30$; $t_d=0.5$; $n=2$; $\epsilon=0.2$; $Gr_c=2$; $Gr=2$; $M=1$; $t=0.5$; $\gamma=1$

Figure 5 indicates that if the value of Peclet number (Pe) increases then concentration of the rarer and lighter component of the binary fluid mixture decreases at any point in the region $[-1, -0.0505]$ while reverse effect is observed at any point in the region $[-0.0505, 1]$. Concentration of the rarer and lighter component of the binary fluid mixture can be increased by increasing the value of Pe .

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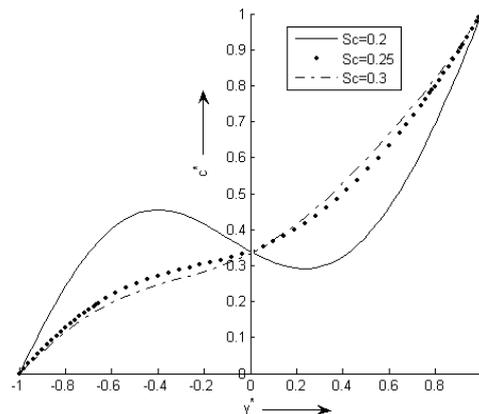


Figure 6: Concentration profile c^* against the width of the channel y^* for different values of Sc and $Re=30$; $t_d=0.5$; $n=2$; $\epsilon=0.2$; $Gr_c=2$; $Gr=2$; $M=1$; $t=0.5$; $\gamma=1$

From the Figure 6 it is clear that the concentration of the rarer and lighter component of the binary fluid mixture decreases gradually in the region $y^* \leq 0$ and then increases in the other half of the channel as the value of Schmidt number (Sc) increases. Thus by increasing the value of Schmidt number (Sc) which depends on kinematic viscosity and mass diffusion can decrease the concentration of the rarer and lighter component of the binary fluid mixture at any point in the region $[-1, 0]$ and can increase the concentration of the rarer and lighter component of the binary fluid mixture at any point in the region $[0, 1]$.

V. CONCLUSION

From the observations it is clear that the non dimensionless parameters Re , γ , t_d , Sc and Pe play important roles in the mass distribution of species of a binary fluid mixture in an unsteady Couette flow between two vertical moving plates. Concentration of the rarer and lighter components of the binary fluid mixture increases as y^* increases from -1 to 1 with the increase in the values of Re , Pe and Sc and concentration of the rarer and lighter component of the binary fluid mixture decreases with the increase in the value of t_d and chemical reaction parameter γ . Thus Re , Pe , Sc enhance the rate of separation and t_d , γ diminish the rate of separation of the rarer and lighter component of the binary fluid mixture.

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